

9555Q

Variable Orifice Cast Iron Double Regulating Valve



Via Circonvallazione, 10
13018 Valduggia (VC), Italy
Tel: +39 0163 47891
Fax: +39 0163 47895
www.vironline.com



Variable orifice cast iron double regulating valve
Flanged PN16 according to EN1092-2 (ex DIN2533)
Lengths according to EN558-1 series 1 (ex DIN3202 F1)
Testing according to EN12266-1
Test points included

PN16

Free of CE marking (cat. according to Art. 4.3 Dir. 2014/68/EU)

Working conditions

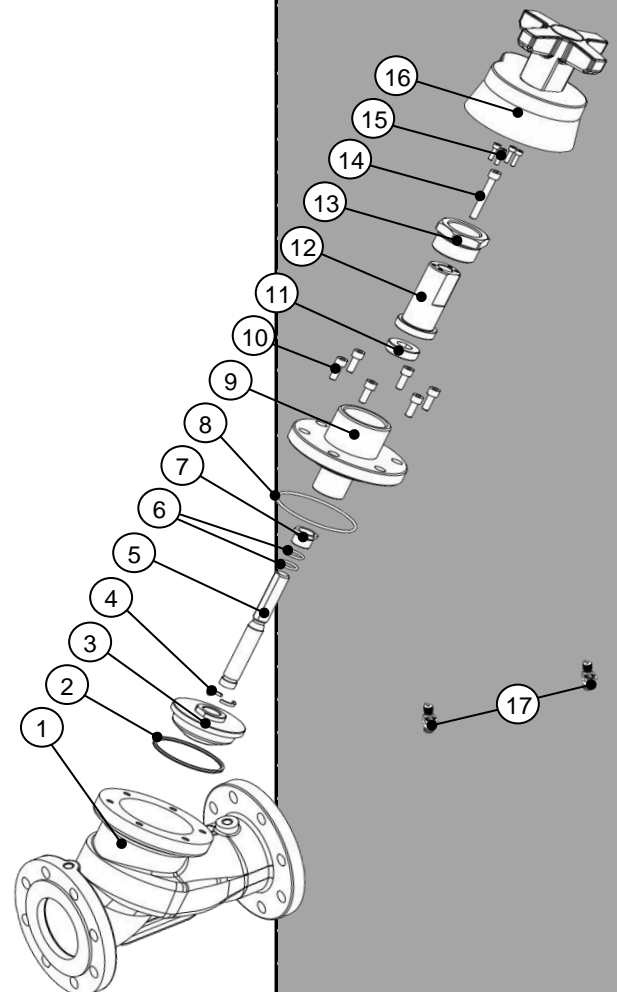
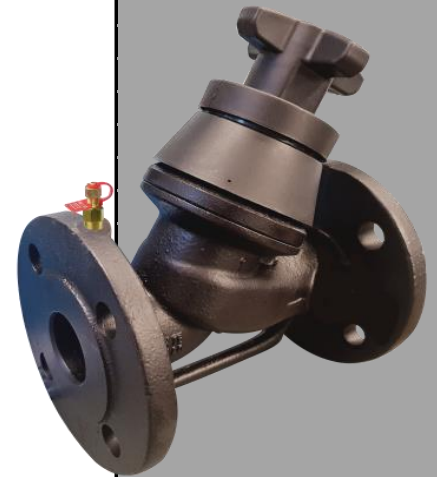
- Suitable for: water, -10°C to +110°C
below 0°C only for water with added antifreeze fluids
over 100°C only for water with added anti-boiling fluids
(ethylene glycol or propylene glycol mixtures up to 50% may be used)
- Not suitable for: gases group 1 & 2, liquids group 1 (Dir. 2014/68/EU)

PARTLIST

N.	Part	Material	Norm
1	Body	Cast iron	EN-GJL-250
2	Cone gasket	EPDM	-
3	Balancing cone	Ductile iron	EN-GJS-400
4	Segment ring	Brass	-
5	Stem	Stainless steel	AISI 420
6	Stem O-ring	EPDM	-
7	Stem bushing	Zinc plated steel	St37
8	Body/bon. O-ring	EPDM	-
9	Bonnet	Cast iron	EN-GJL-250
10	Screws	Zinc plated steel	-
11	Ring	Brass	-
12	Yoke nut	Brass	-
13	Bushing	Zinc plated steel	St37
14	Memory stop	Stainless steel	-
15	Handwheel screw	Stainless Steel	-
16	Handwheel	Polyamide ¹	-
17	Test point	DZR Brass ²	EN12164 CW602N

¹Ductile iron for DN200

²Test points with EPDM gaskets and polypropylene ties

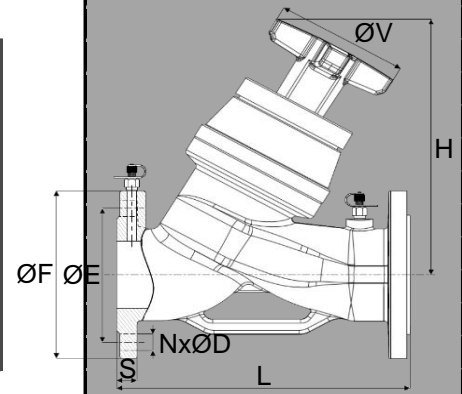


DIMENSIONS

DN	ØF [mm]	ØE [mm]	S [mm]	NxØD [mm]	L [mm]	H [mm]	ØV [mm]	Weight [kg]	Flow range ¹ [l/s]
040	150	110	18	4x19	200	176	86	8,7	0,81-1,88
050	165	125	20	4x19	230	190	86	11,6	1,52-3,51
065	185	145	20	4x19	290	214	86	15,8	3,02-6,95
080	200	160	22	8x19	310	225	86	20,5	6,40-15,36
100	220	180	24	8x19	350	334	160	36,5	10,85-26,04
125	250	210	26	8x19	400	388	160	69,2	16,85-39,75
150	285	240	26	8x23	480	403	160	95,6	23,71-56,91
200	340	295	30	12x23	600	825	400	182,0	41,86-100,47

¹Suggested flow range applicability (BS7350)

If used with measuring manometers different from those proposed by VIR please verify that sensibility of the measuring device is compatible with indicated minimum flow (see flow measurement paragraph)



FLOW MEASUREMENT

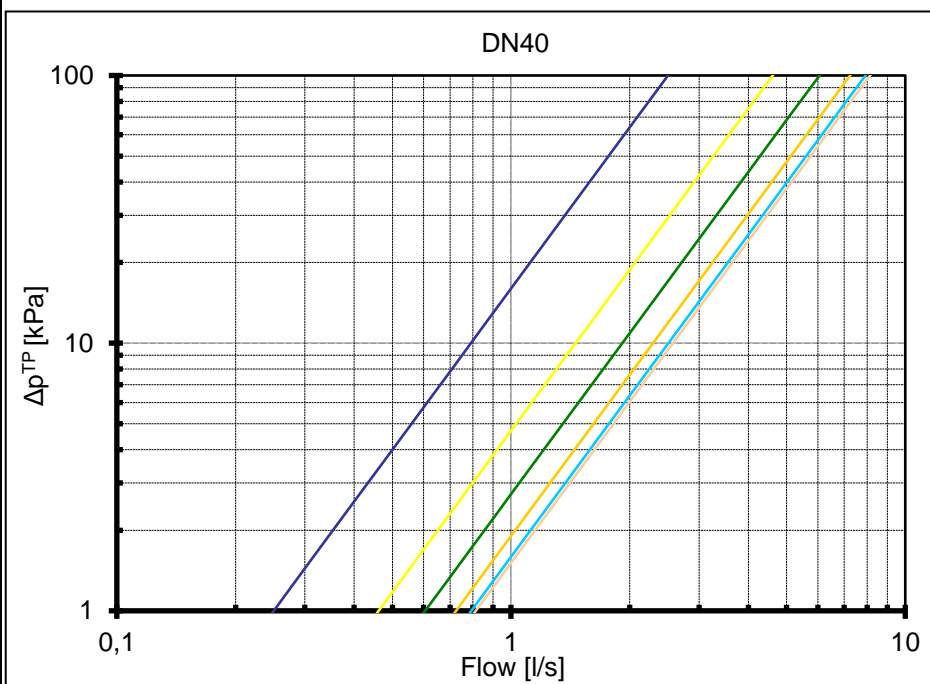
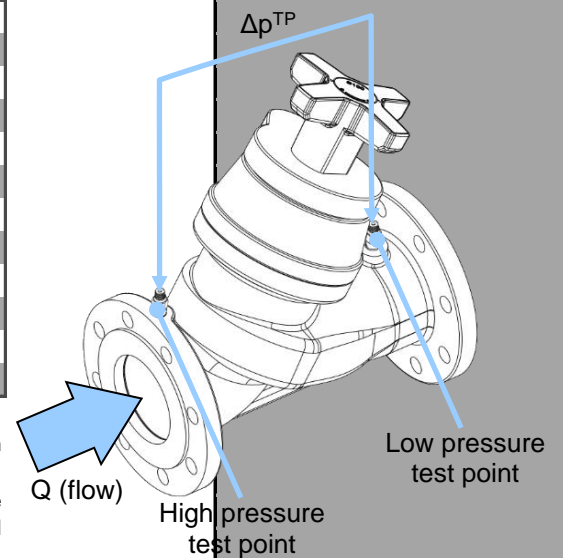
Handwheel position	K _v [m ³ /h @ 1bar]							
	040	050	065	080	100	125	150	200
1,0	9,0	7,7	10,1	10,1	25,2	44,4	21,1	24,7
2,0	16,6	11,5	18,2	18,4	38,5	78,1	31,4	129,3
3,0	21,8	15,6	30,6	26,5	55,3	104,9	40,9	214,7
4,0	26,1	25,1	45,8	42,7	86,8	137,4	52,5	317,0
5,0	28,5	34,2	57,6	66,5	125,0	176,5	90,2	442,3
6,0	29,3	41,1	66,2	85,3	154,4	217,4	152,4	488,0
7,0	-	45,7	69,5	97,6	177,1	257,4	214,9	560,5
8,0	-	47,7	72,0	103,7	185,9	288,1	275,1	657,0
9,0	-	-	-	-	-	300,7	325,2	714,0
10,0	-	-	-	-	-	307,9	355,4	738,7
11,0	-	-	-	-	-	-	-	762,0
12,0	-	-	-	-	-	-	-	790,0

Formula linking flow Q (in l/s) and Δp measured at test points (in kPa). K_v depends on handwheel position as indicated on table.

$$Q = \frac{K_v \cdot \sqrt{\Delta p^{TP}}}{36}$$

Minimum flow that can be measured for each diameter may be calculated by using in the formula minimum Δp that can be measured by used manometer.

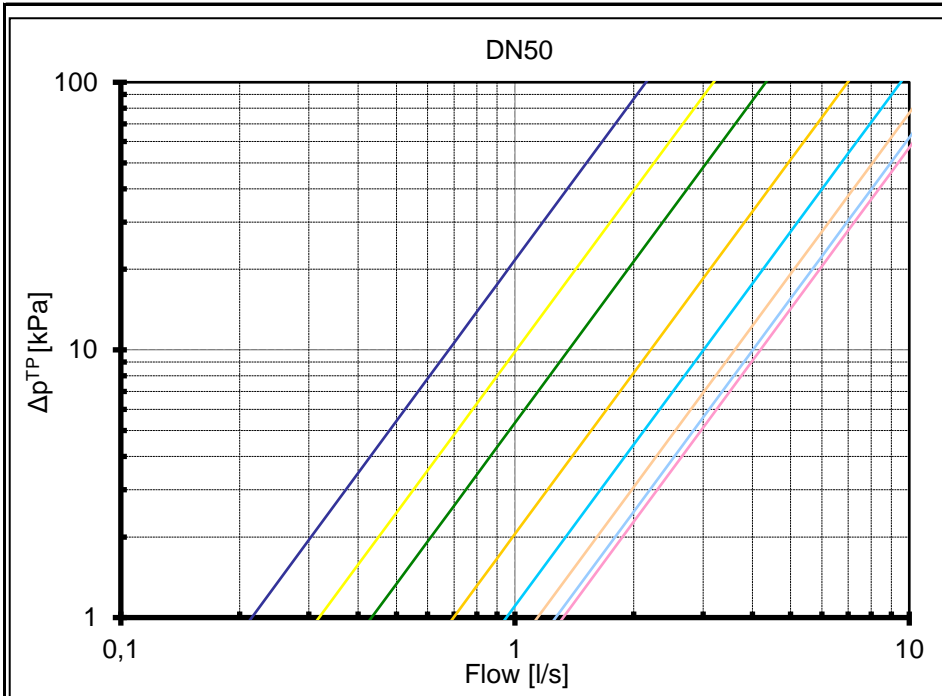
Valves are anyway designed for best performances when used on range previously suggested and as indicated by BS7350.



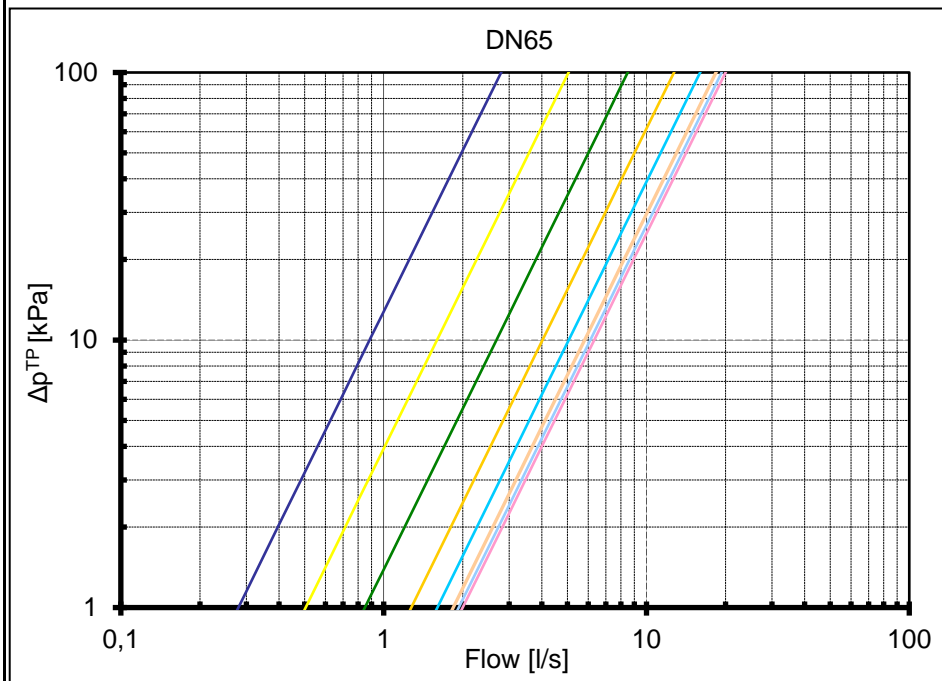
- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0



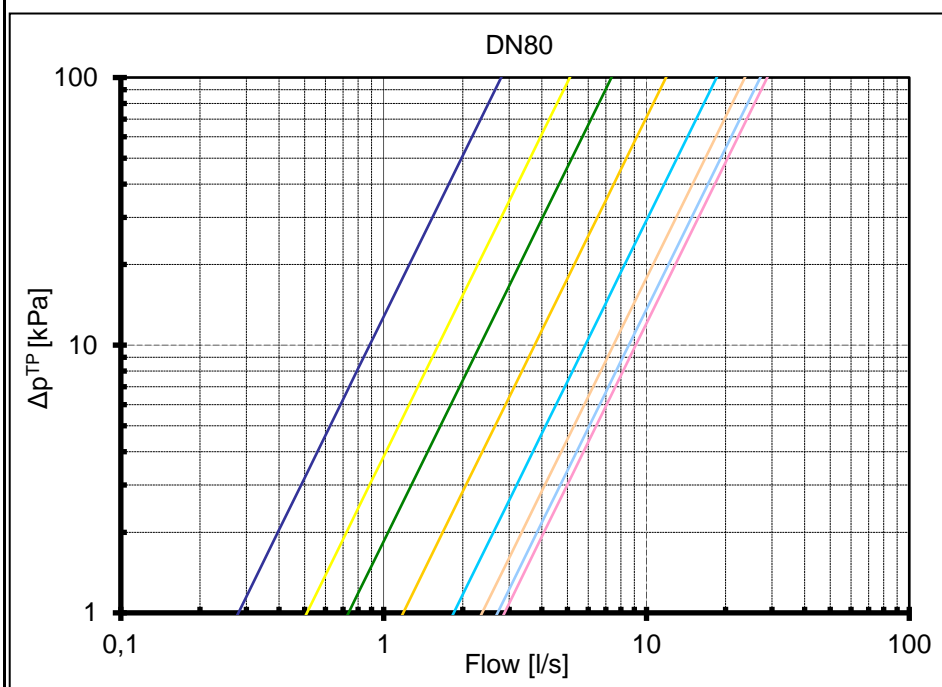
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- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0



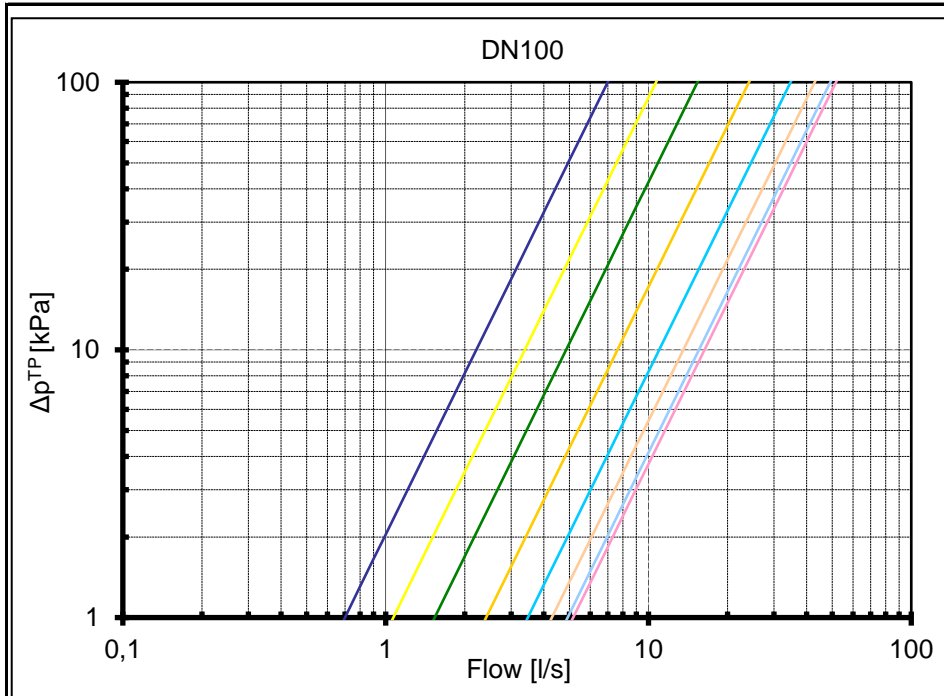
- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0



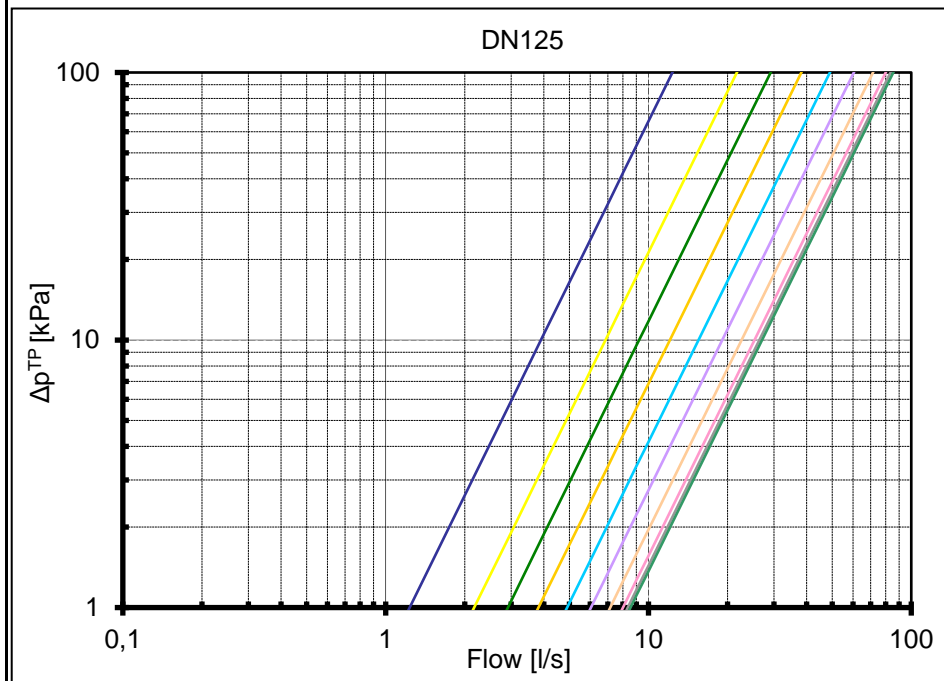
- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0



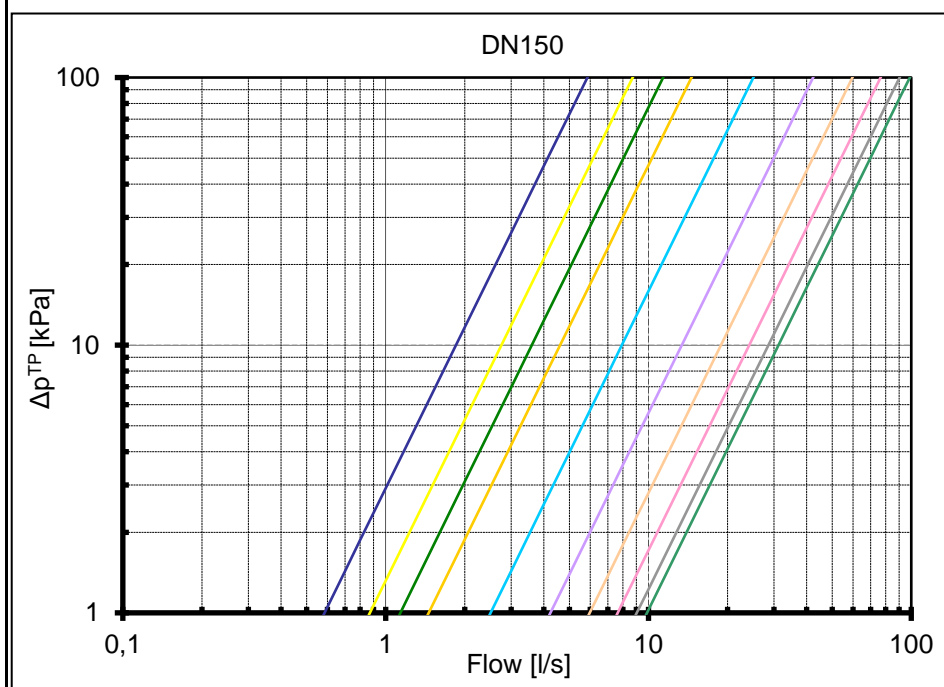
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- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0



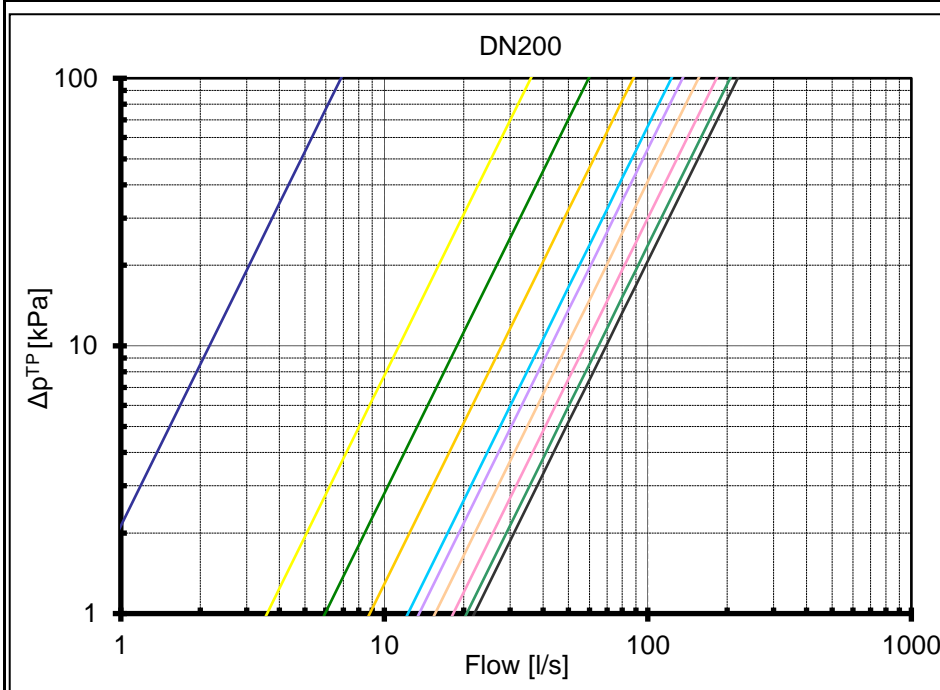
- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0
 - 9,0
 - 10,0



- Handwheel position
- 1,0
 - 2,0
 - 3,0
 - 4,0
 - 5,0
 - 6,0
 - 7,0
 - 8,0
 - 9,0
 - 10,0



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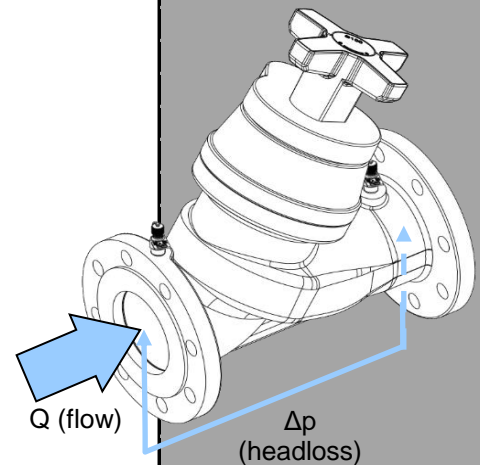
Handwheel position

- 1,0
- 2,0
- 3,0
- 4,0
- 5,0
- 6,0
- 7,0
- 8,0
- 10,0
- 12,0

HEADLOSS CALCULATION

Handwheel position	K _v [m ³ /h @ 1bar]							
	040	050	065	080	100	125	150	200
1,0	9,0	7,7	10,1	10,1	25,2	44,4	21,1	24,7
2,0	16,6	11,5	18,2	18,4	38,5	78,1	31,4	129,3
3,0	21,8	15,6	30,6	26,5	55,3	104,9	40,9	214,7
4,0	26,1	25,1	45,8	42,7	86,8	137,4	52,5	317,0
5,0	28,5	34,2	57,6	66,5	125,0	176,5	90,2	442,3
6,0	29,3	41,1	66,2	85,3	154,4	217,4	152,4	488,0
7,0	-	45,7	69,5	97,6	177,1	257,4	214,9	560,5
8,0	-	47,7	72,0	103,7	185,9	288,1	275,1	657,0
9,0	-	-	-	-	-	300,7	325,2	714,0
10,0	-	-	-	-	-	307,9	355,4	738,7
11,0	-	-	-	-	-	-	-	762,0
12,0	-	-	-	-	-	-	-	790,0

Copy of the table presented in flow measurement paragraph
 Δp (headloss) approximately equal to Δp^{TP}

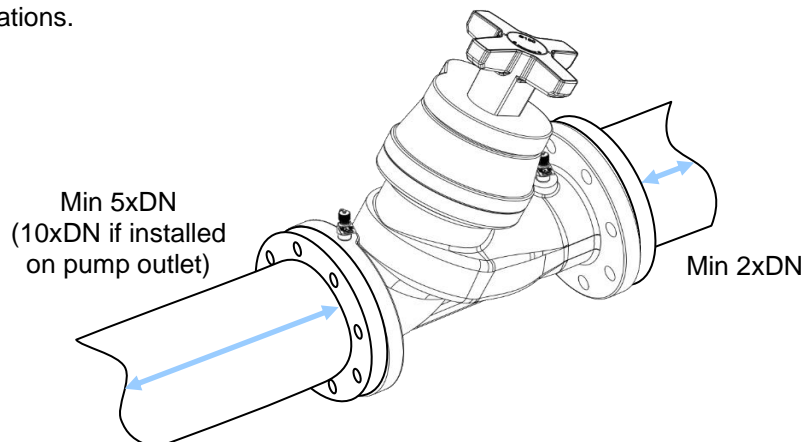


$$\Delta p = \left(\frac{36 \cdot Q}{K_v} \right)^2$$

Formula linking flow Q (in l/s) and theoretical valve headloss Δp (in kPa).
 K_v depends on handwheel position as indicated on table.

INSTALLATION

To obtain the best performances valve must be installed on a pipe with its same nominal size preceded and followed by straight pipe lengths as per figure indications.



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